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Performance analysis of a residential heating system using borehole heat exchanger coupled with solar assisted PV/T heat pump

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Abstract

Borehole heat exchanger (BHE) is a promising method for extracting heat from the deep geothermal energy which has been widely used for residential heating in high latitude areas. The solar assisted photovoltaic/thermal (PV/T) heat pump could convert solar energy into useful heat efficiently, and could be further used to heat water from the BHE to a higher temperature level. In this paper, a residential heating system using BHE coupled with solar assisted PV/T heat pump is therefore proposed with further performance analysis. The simulation results show that a larger mass flow rate could increase the BHE's heat extract capacity but also increase the flow resistance and pump power under nominal conditions. The circulating water would not extract heat from rock-soil if the inlet temperature exceeds 48.5 °C when mass flow rate is 12 kg/s. Furthermore, the maximum water temperature from this hybrid system could reach 40.8 °C while the solar fraction is 67.5% when the area of PV/T module is 1000 m², solar irradiation is 600 W/m² and depth of the BHE is 2500 m. In the meantime, the heating COP of this hybrid system could reach 7.4 and the system could operate independently without power input from electrical grid.

Keywords: Borehole heat exchanger; Solar energy; PV/T; Heat pump; Residential heating

1 Introduction

Nowadays, total energy consumption is constantly climbing and has brought energy and environmental crises due to the combustion of fossil fuels, such as coal and oil. The usage of clean and renewable resources is being considered and developed as an effective way to replace conventional energy resources in recent years [1]. The problem of high and inefficient energy consumption for residential heating in high latitude areas has drawn increasing attention to the community. Geothermal energy is a promising residential heating source due to its high efficiency, low energy consumption, and environmental-friendly [2-4].

Fig. 1 shows the categories and development history of the residential heating system using a borehole heat exchanger. Firstly, the ground source heat pump system is proposed to utilize shallow geothermal energy. Then the deep borehole heat exchanger is developed to avoid ecological damage from the shallow ground source heat pump. Furthermore, as shown in Fig. 1, it is seen from

Categories 1 to 4, the combination of other renewable energy and BHE has been studied recently to improve the system performance.

As shown in Fig. 1, the shallow geothermal energy has been widely used for residential heating or hot water applications by adopting a ground source heat pump system. However, the long-term operation of the shallow ground source heat pump will make the soil temperature imbalance and affect the ecological environment. In fact, the typical geothermal gradient is about $0.03\text{ }^{\circ}\text{C}/\text{m}$ [5] which means the temperature difference of a 2500 m borehole could reach $75\text{ }^{\circ}\text{C}$, thus, the deep borehole heat exchanger has been proposed to extract heat from deep rock-soil layer to overcome the disadvantages of shallow geothermal extraction devices. For instance, Bu et al. [6] demonstrated the feasibility of extracting heat from existing abandoned oil and gas wells by using a deep borehole heat exchanger (4000 m). They developed a mathematical model of the BHE and found that the heat capacity of a single well could reach 454 kW for a geothermal gradient of $25\text{ }^{\circ}\text{C}/\text{km}$ when the inlet velocity is 0.05 m/s . The borehole heat exchanger is the core of the system because the working fluid in BHE could extract heat from the deep ground. Many projects using BHE systems had been constructed in several countries. A 2786 m BHE was adopted to extract heat for domestic hot water and spacing heating in Germany while the other project used a 2500 m BHE in sandstone to provide heat for a building in RWTH-Aachen University [7]. In the case study of Hinton (Alberta), Hu et al. [8] revealed the potential for geothermal exploitation using borehole heat exchangers in the Western Canadian Sedimentary Basin numerically. Their simulation results show that a 3500 m BHE system could produce the heat of 380 kW, and the temperature increment could reach $8.97\text{ }^{\circ}\text{C}$ when the inlet water temperature is $20\text{ }^{\circ}\text{C}$ and the mass flow rate is 10 kg/s .

The BHE has different types including U-shaped, double U-shaped, W-shaped, spiral-shaped, and coaxial [9-11]. Focus on the coaxial deep borehole heat exchanger, numerous researches have been conducted recently. For instance, Renaud et al. [12] numerically simulated a deep BHE in the Krafla geothermal system. They found that the cooling perturbation near the bottom hole is shown to grow radially from 10 to 40 m between 1 and 10 years of production, and the calculated output power reaches up to 1.2 MW for a single well. Luo et al. [13] designed a deep coaxial BHE for harvesting geothermal energy and proposed an analytical model for thermal analysis. They demonstrated the best flow direction with annulus as an inlet in heat extraction mode and confirm the positive influence of increasing geothermal gradients towards the heat extraction. Fang et al. [14] proposed a computationally efficient numerical model for heat transfer simulation of deep borehole heat exchangers, and their results show that the heat production could reach 310 kW for a 2500 m BHE when the geothermal gradient is $30\text{ }^{\circ}\text{C}/\text{km}$ and the geothermal heat flux is $2\text{ W}/\text{m}\cdot^{\circ}\text{C}$. For the medium-deep borehole heat exchanger, Liu et al. [15] developed a transient heat transfer model, and numerically investigated the influence of different parameters on system performance. Their simulation results indicated that the geothermal gradient affects the thermal extraction load mostly and the heat capacity has the greatest impact on the thermal effect radius. Song et al. [16] conducted a numerical analysis of the heat extraction performance of a deep coaxial borehole heat exchanger system and established an unsteady-state heat transfer model. The further study indicated that in terms of the pressure drop and thermal power, the $25\text{ m}^3/\text{h}$ is the optimal flow rate which could obtain the best thermal performance of the BHE (5000 m).

However, the temperature of outlet circulating water could not reach over $40\text{ }^{\circ}\text{C}$ for stable, comfortable residential heating if the inlet water temperature or geothermal gradient is low. Therefore, the combinations of other heat sources (aerothermal, solar energy, etc.) and BHE [17]

85 have been proposed to reach higher outlet water temperature as shown in Fig. 1 (Categories 1 to 4).
86 For instance, Wang et al. [18] conducted a field test and numerical investigation on the heat transfer
87 characteristics and optimized the design of a deep BHE assisted heat pump system (Category 1).
88 Under given conditions, the results from the field test indicated that the average heat transfer
89 capacity of every single borehole and the average COP (coefficient of performance) of the DBGSHP
90 (deep borehole ground source heat pump) heating system were 286.4 kW and 4.6, respectively. The
91 borehole heat exchanger coupled with an air source heat pump system is another method to increase
92 outlet water temperature from BHE. Nevertheless, the deep borehole heat exchanger assisted heat
93 pump system and borehole heat exchanger coupled with the air source heat pump system would
94 consume high compressor power and then leads to a lower coefficient of performance.

95 Major studies focus on the borehole heat exchanger assisted heat pump system (Fig. 1,
96 Category 1). In addition to the ground source heat pump system, utilization of solar energy (Fig. 1,
97 Category 3,4) is another effective method to widen the application of the BHE coupled heat pump
98 system [19]. As shown in Fig. 1, in the borehole heat exchanger coupled with solar collector system
99 (Category 3), a solar flat-plate collector has been used to absorb solar heat and further heat the outlet
100 water from BHE. For instance, Ozgener and Hepbasli [20, 21] experimentally analyzed a solar
101 assisted ground source heat pump heating system. In their study, the heating COP of the ground
102 source heat pump unit and the overall system are obtained to be 2.64 and 2.38, respectively. Wang
103 et al. [22] presented a novel hybrid solar ground source heat pump system for office building heating.
104 For the proposed HSGSHPS, the electrical energy demand of the system could be reduced by 32%
105 if the load circulation pump is operated based on the fan-coils rather than always-on operation.
106 Nevertheless, the direct expansion solar assisted heat pumps could produce heat more stable
107 compared with the solar collectors used in these systems. Thus, the combination of direct expansion
108 solar assisted heat pumps could be a more effective and stable way to heat the outlet water from
109 BHE for residential heating.

110 In this paper, a novel borehole heat exchanger coupled with a solar assisted PV/T heat pump
111 has been proposed. The configuration of this novel hybrid system is presented in Fig. 2. A
112 mathematical model of this hybrid system is developed and the model of BHE is validated by
113 experiment. The performance of this hybrid system has been studied.

Fig. 1. Categories and development history of the residential heating system using borehole heat exchanger.

2 System description

2.1 System configuration

Fig. 2 shows the schematic diagram of a residential heating system using a deep borehole heat exchanger (BHE) coupled with a solar assisted PV/T heat pump. This system has three main parts: borehole heat exchanger, solar assisted PV/T heat pump, and solar power unit. The borehole heat exchanger has two coaxial pipes: inner and outer pipes to form the inlet and outlet fluid channel. The depth of the BHE is 2500 m, and the circulating water will flow deep into the BHE's bottom and extract heat from the rock-soil. The other part is the solar assisted PV/T heat pump which could increase the water temperature from the BHE because the outlet water temperature from BHE may not meet the temperature for residential heating applications. The solar assisted PV/T heat pump system consists of PV/T collector/evaporator, compressor, condenser, and expansion valve. The PV/T collector/evaporator could produce electricity and heat simultaneously. The solar power unit consists of MPPT solar energy controller, accumulator, and AC-DC inverter. The electricity from solar PV/T panel could be used to drive the compressor and circulating pump and the surplus electricity could output to the electrical grid.

This system can be operated with three operating modes:

(1) Borehole heat exchanger mode: The solar assisted PV/T heat pump would be stopped when the solar radiation is poor or during the night, and only the borehole heat exchanger is operated. The deep BHE will operate during day and night because it would not be influenced by the ambient conditions. Valve 1 is closed while valve 2 is opened and the circulating pump works uninterruptedly

in this mode.

(2) Solar assisted PV/T heat pump mode: The heat from solar assisted PV/T heat pump system would meet the residential heating demand when the insolation is good enough. Therefore, the borehole heat exchanger could be turned off. Valve 1 is opened while valve 2 is closed and the electricity output by PV panel could be used to drive the compressor.

(3) Hybrid mode: If operating the BHE or solar assisted PV/T heat pump alone would not meet the residential heating demand, these two sub-systems would be operated simultaneously. Valve 1 is closed while valve 2 is opened and both the compressor and the pump would work uninterruptedly. The low-temperature water would be heated up to a middle-temperature level firstly by the borehole heat exchanger and then be heated up to a high-temperature level by solar assisted PV/T heat pump. In the meantime, the electricity output by PV panels could be used to drive the compressor and pump.

Fig. 2. Schematic diagram of a residential heating system using borehole heat exchanger coupled with a solar assisted PV/T heat pump.

The values of the chosen parameters are taken in the field tests from the references [7, 18, 23] for initial simulation. The basic specifications for this hybrid system are listed in Table. 1.

Table. 1. The basic specifications for the system.

Parameters	Nomenclature	Value	Unit
Radius of construction hole	r	0.1	m
Inner radius of inner pipe	r_1	0.045	m
Outer radius of inner pipe	r_2	0.055	m
Inner radius of outer pipe	r_3	0.080	m
Outer radius of outer pipe	r_4	0.089	m
Number of BHE	n	1	[-]
Depth of BHE	H	2500	m
Heat transfer fluid in BHE	$[-]$	water	[-]
Mass flow rate of circulating fluid	m	12	kg/s
Inlet water temperature to BHE	T_i	30	°C
Area of PV/T module	A	1000	m ²
Circulating pump power	W_{pump}	17.3	kW
Compressor power	W_{comp}	56.4	kW

2.2 Performance indices

The performance of this hybrid residential heating system is determined by its two sub-systems: borehole heat exchanger and solar assisted PV/T heat pump. The performance of the borehole heat exchanger would be influenced by the mass flow rate, inlet water temperature, depth of BHE, the radius of inner and outer pipe. The performance of solar assisted PV/T heat pump would be influenced by solar radiation intensity, area of PV/T module. Therefore, the performance indices should be defined to evaluate the system performance, which have been listed as follows.

For borehole heat exchanger:

- (1) Q_{BHE} , kW: Heat extract capacity of BHE and it could be expressed as:

$$Q_{BHE} = C_{pf} \cdot m_f \cdot (T_{out} - T_{in}) \quad (1)$$

where C_{pf} is the specific heat at constant pressure, kJ/kg·°C; m_f is the circulating water mass flow rate, kg/s;

- (2) T_{in} , T_{out} , °C: Inlet and outlet water temperature.

- (3) T_{dif} , °C: Temperature difference between inlet and outlet circulating water and it could be calculated by:

$$T_{dif} = T_{out} - T_{in} \quad (2)$$

- (4) R , m: Thermal effect radius of BHE and it reflects the boundary to which the BHE could extract heat form rock-soil.

- (5) COP_{BHE} : Coefficient of performance of BHE and it could be defined as:

$$COP_{BHE} = Q_{BHE} / W_{pump} \quad (3)$$

- (6) P_{dif} , kg/cm²: Water pressure difference between inlet and outlet, and it could be calculated by:

$$P_{dif} = P_{in} - P_{out} \quad (4)$$

where P_{in} , P_{out} are the water pressures in the inlet and outlet, kg/cm².

(7) H_{res} , m: Corresponding water head caused by flow resistance and it could be calculated by:

$$H_{res} = P_{dif} / \rho \quad (5)$$

where ρ is the water density, kg/m³.

(8) W_{pump} , kW: Circulating pump power and it could be calculated by:

$$W_{pump} = m_f \cdot g \cdot H_{res} \quad (6)$$

For solar assisted PV/T heat pump:

(1) COP_{hp} : Coefficient of performance of solar assisted PV/T heat pump and it could be defined as:

$$COP_{hp} = Q_{cond} / W_{comp} \quad (7)$$

(2) Q_{cond} , kW: Condensation heat of heat pump.

(3) W_{comp} , kW: Compressor power.

(4) η_{th} : Thermal efficiency of PV/T collector and it could be calculated by:

$$\eta_{th} = Q_{eva} / (I \cdot A) \quad (8)$$

(5) η_e : Electrical efficiency of PV panels and it could be calculated by:

$$\eta_e = Q_e / (I \cdot A) \quad (9)$$

For hybrid system:

(1) $Q_{heating}$, kW: Heating capacity and it is the sum of Q_{BHE} and Q_{cond} .

(2) COP_{sys} : Coefficient of performance of this hybrid system and it could be defined as:

$$COP_{sys} = (Q_{BHE} + Q_{cond}) / (W_{pump} + W_{comp}) \quad (10)$$

3 Mathematical model

3.1 Borehole heat exchanger

As shown in Fig. 2, the borehole heat exchanger is an important component of this hybrid heating system and its physical model has been presented in detail in Fig. 3. This coaxial borehole heat exchanger has a concentric structure and consists of inner and outer pipes. Moreover, the gap between inner and outer pipes is the inlet fluid channel while the inner pipe is the outlet fluid channel.

An analytical method was used to solve the heat transfer model of the borehole heat exchanger and the following assumptions were made to simplify the analysis:

1. The ground has homogeneous properties.
2. The ground thermal and physical properties are constant during system operation.
3. Underground water flow and the effect of groundwater were not considered.
4. The heat capacities of inner and outer pipes were neglected and the heat transfer state was considered steady.
5. Ground temperature at far boundary remains constant.

6. The axle wire of the borehole heat exchanger was considered as an adiabatic boundary.
7. The longitudinal heat transfer process was neglected.

Fig. 3. Cross-section view of a deep borehole heat exchanger physical model.

According to the above-mentioned assumptions, the heat transfer model of a BHE differential unit, which is shown in Fig. 4, has been developed. The height of this BHE unit is dz and this unit could be separated into five units: outlet fluid differential unit, inner pipe differential unit, inlet fluid differential unit, outer pipe differential unit, and ground differential unit. The heat transfer process of each unit has been detailed in Fig. 3 while the coordinate system is established in Fig. 4, and the origin of the coordinate is the bottom of the BHE.

Fig. 4. Heat transfer model of a BHE differential unit.

The heat transfer rate from inlet fluid differential unit to outlet fluid differential unit through the inner pipe is Q_1 which can be calculated by [24]:

$$Q_1 = \frac{2\pi dz (T_{f2} - T_{f1})}{\frac{1}{\alpha_1 r_1} + \frac{1}{k_1} \ln \frac{r_2}{r_1} + \frac{1}{\alpha_2 r_2}} = \frac{2\pi dz (T_{f2} - T_{f1})}{R} \quad (11)$$

where t_{f1} and t_{f2} are the outlet and inlet water temperatures, respectively; α_1 is the convective heat transfer coefficient between outlet water and inner pipe; α_2 is the convective heat transfer coefficient between inlet water and inner pipe; k_1 is the thermal conductivity of inner pipe; r_1 to r_4 are the inner and outer radiuses of inner and outer pipes; R is the entire thermal resistance between outlet water and inlet water.

The heat gain of outlet fluid differential unit can be expressed as:

$$Q_2 = \rho_f C_{pf} \frac{\partial T_{f1}}{\partial z} dz \cdot \pi r_1^2 v_1 \quad (12)$$

where ρ_f is the density of water; C_{pf} is the specific heat at constant pressure; v_1 is the outlet velocity of the water.

According to the conservation of energy, all the heat transferred from other differential units to outlet differential unit should equal to the increment of the outlet fluid differential unit:

$$Q_1 = Q_2 \quad (13)$$

Eliminate πdz from the formula and then the governing equation for the outlet fluid differential

unit can be expressed as:

$$\frac{2}{R}(T_{f_2} - T_{f_1}) - \rho_f C_{pf} \frac{\partial T_{f_1}}{\partial z} r_1^2 v_1 = 0 \quad (14)$$

The heat transfer rate from the outer pipe to the inlet fluid differential unit can be calculated by:

$$Q_3 = \frac{2\pi dz \cdot (T_3 - T_{f_2})}{\alpha_3 r_3} \quad (15)$$

where t_3 is the temperature of the outer pipe; α_3 is the convective heat transfer coefficient between the outlet water and the outer pipe;

According to the assumptions, only the radial heat transfer process is considered, thus:

$$Q_4 = -Q_1 \quad (16)$$

$$Q_6 = -Q_3 \quad (17)$$

The heat gain of the inlet fluid differential unit can be expressed as:

$$Q_5 = -\rho_f C_{pf} \pi (r_3^2 - r_2^2) v_2 \cdot \frac{\partial T_{f_2}}{\partial z} \cdot dz \quad (18)$$

According to the conservation of energy, this equation can be obtained:

$$Q_3 + Q_4 = Q_5 \quad (19)$$

Then submit Q_3 , Q_4 , Q_5 into the equation, and the governing equation for the inlet fluid differential unit can be expressed as:

$$2\alpha_3 (T_3 - T_{f_2}) + \frac{2(T_{f_1} - T_{f_2})}{R} = -\rho_f C_{pf} (r_3^2 - r_2^2) v_2 \frac{\partial T_{f_2}}{\partial z} \quad (20)$$

The boundary conditions for solving this heat transfer model of BHE are obtained from reference [15] and listed in Table. 2.

Table. 2. Boundary conditions for the BHE differential unit.

Position	Expression	Equation
Fluid inlet	$Z = H$	$T_{f_2} = T_i$
Bottom of the BHE	$Z = 0$	$T_{f_2} = T_{f_1}$
Axle wire	$r = 0$	$Q = 0$
Far ground boundary	$r \rightarrow \infty$	$T_{ground} = T_\infty$

The properties of the borehole heat exchanger listed in Table. 3 are selected as typical values for initial simulation according to the references [5, 7, 18, 23].

Table. 3. Properties of the borehole heat exchanger.

Parameters	Nomenclature	Value	Unit
specific heat at constant pressure of water	C_{pf}	4.2	$\text{kJ/kg}\cdot^\circ\text{C}$
Inner pipe material	$[-]$	PE	$[-]$
Thermal conductivity of inner pipe	k_l	0.4	$\text{W/m}\cdot^\circ\text{C}$
Outer pipe material	$[-]$	Seamless stell J55	$[-]$
Thermal conductivity of outer pipe	k_2	41	$\text{W/m}\cdot^\circ\text{C}$
Thermal conductivity of the ground	k_g	3.49	$\text{W/m}\cdot^\circ\text{C}$
Depth of BHE	H	2500	m
Mass flow rate of circulating water	m	12	kg/s
Ambient temperature	T_a	10	$^\circ\text{C}$
Ground surface temperature	T_{up}	10	$^\circ\text{C}$
Geothermal gradient	T_g	0.03	$^\circ\text{C/m}$
Inlet water temperature to BHE	T_i	30	$^\circ\text{C}$

3.2 PV/T collector/evaporator

Fig. 5 shows the heat loss and physical model of a typical PV/T collector/evaporator. A portion of the solar radiation can be converted to electricity directly by PV panels while the PV panel would absorb the rest of solar radiation and convert it to heat. The PV/T technology could output both electricity and heat simultaneously and is suitable for heating applications.

Fig. 5. Heat loss and physical model of PV/T collector/evaporator [25].

The electricity output by PV panels could be expressed as:

$$Q_e = A \cdot I \cdot \tau_{g,pv} \cdot \alpha_p \cdot \beta_p \cdot \eta_e \quad (21)$$

where A is the area of PV/T module; I is the solar radiation intensity; $\tau_{g,pv}$ is the transmittances of the PV-glazing cover; α_p is the absorption ratio of the PV panels; β_p is the packing factor of PV panels; η_e is the PV panels' efficiency which can be calculated by [26]:

$$\eta_e = \eta_{rc} \cdot \left[1 - \beta_{pv} \cdot (T_p - T_{rc}) \right] \quad (22)$$

η_{rc} is the reference photovoltaic efficiency value of PV panels at $T_{rc}=298$ K, $\eta_{rc}=0.18$; β_{pv} is the temperature coefficient (1/K) of PV cell efficiency, $\beta_{pv}=0.0045$ [26].

The heat absorbed by the PV/T module can be calculated by [27]:

$$Q_{eva} = A \cdot F' \cdot [(\tau_{g,pv} \cdot \alpha_p \cdot \beta_p) \cdot I \cdot (1 - \eta_e) - U_L \cdot (T_w - T_a)] \quad (23)$$

where F' is the efficiency factor; T_w is the average refrigerant temperature in the PV/T collector/evaporator; T_a is the ambient temperature; U_L is the overall heat loss coefficient which can be expressed as:

$$U_L = \left[1 / (h_{cv,p-c} + h_{rd,p-c}) + 1 / (h_{cv,c-a} + h_{rd,c-a}) \right]^{-1} \quad (24)$$

$h_{cv,p-c}$ and $h_{rd,p-c}$ are the convective and radiative heat-transfer coefficients between PV panels and glass cover; $h_{cv,c-a}$ and $h_{rd,c-a}$ are the convective and radiative heat-transfer coefficients between the glass cover and ambient.

The characteristics of different PV/T layers are obtained from the reference [25] and listed in Table. 4.

Table. 4. Characteristics of different PV/T layers [25].

Parameters	Nomenclature	Value	Unit
Thickness of PV-glazing cover	$\delta_{g,pv}$	1	mm
Emissivity of PV-glazing cover	ε_c	0.84	[-]
Transmissivity of PV-glazing cover	$\tau_{g,pv}$	0.9	[-]
Thickness of PV cells	δ_{pv}	0.3	mm
Emissivity of PV cells	ε_p	0.96	[-]
Absorptance of PV cells	α_p	0.85	[-]
Thermal conductivity of PV cells	κ_p	203	W/m·°C
Absorptance of PV baseboard	α_b	0.8	[-]
Thickness of EVA grease	δ_{EVA}	0.5	mm
Thermal conductivity of EVA grease	κ_{EVA}	0.311	W/m·°C
Thickness of electrical insulation	δ_{ei}	0.5	mm
Thermal conductivity of electrical insulation	κ_{ei}	0.15	W/m·°C
Electrical insulation material	[-]	Tedlar	[-]
Packing factor	β_p	1	[-]
Length of PV/T collector/evaporator	L	2.0	m
Width of PV/T collector/evaporator	W	1.0	m
Area of the PV/T collector/evaporator	A	2.0	m ²
Thermal conductivity of roll-bond panel	κ_{rb}	151	W/m·°C
Thickness of roll-bond panel pipe	δ_{rb}	1	mm
Refrigerant type	ref	R134a	[-]

3.3 Compressor

The refrigerant mass flow rate m_{ref} in the thermodynamic cycle can be calculated by [28]:

$$m_{ref} = \lambda \cdot V_{th} / v_{suc} \quad (25)$$

where the λ is the compressor volumetric efficiency, V_{th} is the theoretical displacement volume of the compressor, v_{suc} is the specific volume of the refrigerant in the suction period.

The power consumption of compressor can be calculated by:

$$P_{com} = m_{ref} \cdot (h_{dis} - h_{suc}) / \eta_{ele} \quad (26)$$

where h_{dis} and h_{suc} are the enthalpies of discharged and suction refrigerant in the compressor, respectively; η_{ele} is the efficiency of the compressor.

The refrigerant vapor through the compressor is isentropic, thus, the equation can be expressed as:

$$T_{dis} / T_{suc} = (p_{dis} / p_{suc})^{(\chi-1)/\chi} \quad (27)$$

where the χ is the polytropic index of refrigerant; p_{dis} and p_{suc} are the pressure of discharged and suction refrigerant in the compressor, respectively.

3.4 Condenser

The heat transferred by refrigerant vapor to condenser can be expressed as:

$$Q_{cond} = m_{ref} \cdot (h_{cond,in} - h_{cond,out}) \quad (28)$$

where $h_{cond,in}$ and $h_{cond,out}$ are the inlet refrigerant enthalpy and outlet refrigerant enthalpy through the condenser, respectively.

In this hybrid system, the condensation heat could be used to heat the outlet water from the borehole heat exchanger for residential heating applications.

3.5 Expansion valve

The refrigerant fluid passes rapidly through the expansion valve, thus, this process is practically considered as adiabatic and isenthalpic in the steady stage. Consequently, the enthalpy of inlet and outlet refrigerant through expansion valve are considered the same which can be expressed as:

$$h_{expan,in} = h_{expan,out} \quad (29)$$

where $h_{expan,in}$ and $h_{expan,out}$ are the inlet refrigerant enthalpy and outlet refrigerant enthalpy through the expansion valve, respectively.

4 Experimental validation

The residential heating system using BHE coupled with solar assisted PV/T heat pump is first proposed in this paper and the experiments of this kind of hybrid system have not been reported. In this hybrid system, the borehole heat exchanger and solar assisted PV/T heat pump are arranged in parallel to heat the circulating water. Thus, these two systems could be validated independently. The mathematical model of the solar assisted PV/T heat pump has been validated in Yao's paper [25]. Therefore, in this section, the experimental results from reference [18] have been used to verify the mathematical model of the BHE system. The experimental setup and properties of the borehole heat exchanger have been listed in Table. 5.

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Table. 5. Experimental setup and properties of the borehole heat exchanger [18].

Parameters	Nomenclature	Value	Unit
Outer diameter of inner pipe	d_2	0.11	m
Thickness of inner pipe	δ_1	0.01	m
Outer diameter of outer pipe	d_4	0.1778	m
Thickness of inner pipe	δ_2	0.00919	m
Circulating fluid	[-]	Water	[-]
Inner pipe material	[-]	HDPE	[-]
Thermal conductivity of inner pipe	k_1	0.45	W/m·°C
Outer pipe material	[-]	Seamless stell J55	[-]
Depth of BHE	H	2000	m
Inlet velocity of circulating water	v_{in}	0.7	m/s
Mass flow rate of circulating water	m	7.32	kg/s

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The experimental and simulated inlet water temperature, inlet velocity of circulating water, outlet water temperature from BHE, and heat extract capacity under typical conditions have been listed in Table. 6. It can be found that the average outlet water temperature from BHE and the heat extract capacity are 26.6 °C and 286.4 kW, respectively, when the average inlet water temperature to BHE is 17.6 °C and the inlet velocity is 0.7 m/s. The simulation is conducted at the same inlet water temperature and inlet velocity. The simulation results show that the outlet water temperature from BHE is 26.3 °C while the heat extract capacity is 267.5 kW. Compared with the experimental results, the relative errors of outlet water temperature from BHE and heat extract capacity are 3.0% and 6.6%, respectively. Both relative errors are under 7% which means the simulation results show good agreement with the experimental results.

Table. 6. Comparison between experimental and simulated results under typical conditions.

Item	Inlet water temperature to BHE (°C)	Inlet velocity of circulating water (m/s)	Outlet water temperature from BHE (°C)	Heat extract capacity (kW)
Experimental results	17.6	0.7	26.6	286.4
Simulation results	17.6	0.7	26.3	267.5
Relative error	[-]	[-]	3.3%	6.6%

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To further ensure the reliability of the mathematical model, the error analyses of experimental and simulated outlet temperatures changing with inlet velocity and inlet temperature have been conducted, and the results have been shown in Fig. 6. The green dots represent the experimental outlet temperatures under different conditions. Fig. 6(a) shows the decreasing trend of outlet temperature with the increase of inlet velocity when the inlet temperature is 17 °C, and the simulated outlet temperature reduces linearly from 32.4 °C to 24.2 °C when inlet velocity varies from 0.3 m/s to 1.3 m/s. The maximum relative error (2.66%) is obtained when the inlet velocity is 0.7 m/s while the average relative error is 1.67%. As shown in Fig. 6(b), the outlet temperature increases with the increase of inlet temperature (13 °C to 23 °C) when the inlet velocity is 0.7 m/s. The peak value of the simulated outlet temperature is 32.2 °C while the experimental outlet temperature is 33.0 °C

when the inlet temperature is 23 °C, and its corresponding relative error is -2.21%. The maximum relative error is 2.94%, which occurs when the inlet temperature is 13 °C, while the experimental and simulated outlet temperatures are 25.4 °C and 26.2 °C, respectively. The average relative error is 1.93% in this case. All the relative errors of experimental and simulated outlet temperatures under different conditions are within $\pm 5\%$, which means the simulation results show good agreement with the experimental results. Therefore, the proposed mathematical model of BHE is considered reliable for further performance analysis.

Fig. 6. Error analyses of (a) experimental and simulated outlet temperatures changing with inlet velocity. (b) experimental and simulated outlet temperatures changing with inlet temperature.

5 Performance analysis

After the validation of the mathematical model, further performance analysis of the proposed residential heating system using a borehole heat exchanger coupled with a solar assisted PV/T heat pump has been conducted. The effects of the system operating conditions (mass flow rate, inlet water temperature, thermal effect radius, solar radiation intensity) and physical structure parameters (inner and outer pipes' diameters, area of PVT module) on system performance have been numerically investigated in this section. Moreover, the feasibility analysis has also been conducted to reveal the merits of this hybrid system.

5.1 Mass flow rate

The influence of mass flow rate instead of inlet velocity on system performance is analyzed in this sub-section. That is because the circulating water is pumped by the circulating pump, and the most important parameter of the pump is the mass flow rate. In addition, different mass flow rate determines different types of circulating pump. However, the inlet velocity needs to be calculated by the mass flow rate and the inlet area. Therefore, it is more reasonable to select the mass flow rate as a variable parameter. The influence of circulating water mass flow rate varying from 8 kg/s to 16 kg/s on water temperature at different positions has shown in Fig. 7. Here the inlet water temperature to BHE is 20 °C and the depth of BHE is 2500 m. The outlet water temperature increases with the decrease of mass flow rate and the outlet water temperature could reach the peak value which is 27.4 °C when the mass flow rate is 8 kg/s. That is because a lower mass flow rate would lead to a

lower inlet velocity which means the circulating water could extract heat from rock-soil sufficiently in the annular fluid channel. The temperature differences between outlet and inlet water are 7.4 °C, 6.3 °C, 5.4 °C, 4.7 °C, and 4.2 °C when the mass flow rates are 8 kg/s, 10 kg/s, 12 kg/s, 14 kg/s and 16 kg/s, respectively. A higher outlet water temperature is more suitable for residential heating, from this aspect, a lower inlet mass flow rate is better for system performance. However, the heat extract capacity is determined by the mass flow rate and temperature difference as shown in Eq. 1. Thus, the heat extract capacity and system COP should be calculated to evaluate the system performance.

Fig. 7. Influence of mass flow rate on circulating water temperature at different positions.

Fig. 8 shows the influence of mass flow rate on the temperature difference between outlet and inlet water, heat extract capacity, and COP_{BHE} . The heat extract capacity increases and the BHE system COP, as well as the temperature difference, decreases with the increase of mass flow rate. For instance, the temperature increment of 8 kg/s is the highest (7.4 °C) but the heat extract capacity under this condition is the lowest (248.8 kW). The heat extract capacity could reach the peak value which is 282.5 kW while the BHE system COP is 7.3 when the mass flow rate is 16 k/s. Compared with a conventional heating system like an air conditioner, the borehole heat exchanger is more efficient, low-energy consumption, and environmental-friendly.

Fig. 8. Influence of mass flow rate on the temperature difference between outlet and inlet water, heat extract capacity, and COP_{BHE} .

The mass flow rate would influence the flow resistance in the fluid channel and then affect the circulating pump power. Fig. 9 reveals the variation trends of corresponding water head, water pressure difference, and circulating pump power with the mass flow rate. These three parameters increase gradually with the increase of mass flow rate. A higher mass flow rate would lead to a higher flow resistance due to turbulence flow and cause a higher circulating pump power. For instance, the pressure difference between inlet and outlet is the highest (2.5 Mpa) and its corresponding water head is 247 m. In the meantime, the circulating pump power is 39 kW which could be calculated by Eq. 5.

Fig. 9. Influence of mass flow rate on corresponding water head, water pressure difference between inlet and outlet, and circulating pump power.

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430 5.2 Inlet water temperature

431 Fig. 10 shows the influence of inlet water temperature on circulating water temperature at
 432 different positions. The circulating water mass flow rate is 12 kg/s and the depth of BHE is 2500 m.
 433 The outlet water temperatures are 13.2 °C, 17.3 °C, 21.3 °C, 25.4 °C, 29.4 °C, 33.5 °C when inlet
 434 water temperatures are 5 °C, 10 °C, 15 °C, 20 °C, 25 °C, 30 °C, respectively. A higher inlet water
 435 temperature leads to a higher outlet water temperature, but the temperature difference between outlet
 436 and inlet water decreases with the increase of inlet water temperature. For instance, the outlet water
 437 temperature is 33.5 °C when the inlet water temperature is 30 °C while the temperature difference
 438 is the lowest (3.5 °C).

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440 **Fig. 10.** Influence of inlet water temperature of BHE on circulating water temperature at different
 441 positions.

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443 Fig. 11 shows the influence of the inlet water temperature of BHE on the temperature difference
 444 between outlet and inlet water, heat extract capacity, and COP_{BHE} . Both heat extract capacity and
 445 BHE system COP decrease linearly with the increase of inlet water temperature. The heat extract
 446 capacity is 176.4 kW while the BHE system COP is 10.2 when the inlet water temperature is 30 °C.
 447 Furthermore, the temperature difference between outlet and inlet water decreases when the inlet
 448 water temperature increases. It is important to reveal the turning point when the temperature
 449 difference between the inlet and the outlet will be to 0 °C because it will reflect the upper-
 450 temperature limit of the inlet water.

Fig. 11. Influence of inlet water temperature of BHE on the temperature difference between outlet and inlet water, heat extract capacity, and COP_{BHE} .

The influence of inlet water temperature (over 40 °C) on outlet water temperature has been further studied. As shown in Fig. 12, the outlet water temperature increases linearly while the temperature difference decreases linearly when inlet water temperature increases. Under this condition, the turning point occurs when the inlet water temperature is 48.5 °C which means the BHE would not produce heat any longer. Moreover, the circulating water will transfer heat to the ground when the inlet water temperature is over 48.5 °C.

Fig. 12. Influence of inlet water temperature (over 40 °C) of BHE on outlet water temperature from BHE and temperature difference between inlet and outlet.

5.3 Inner and outer pipes' diameters

The inner and outer pipes diameter would affect the flow resistance in the fluid channel and then influence the thermal performance of BHE as well as the circulating pump power. Fig. 13(a) shows the influence of the inner pipe diameter on the temperature difference between outlet and inlet, heat extract capacity, and BHE system COP. The outer pipe diameter is 0.178 m, circulating water mass flow rate is 12 kg/s, inlet water temperature to BHE is 20 °C, and depth of BHE is 2500 m. The variation of outlet and inlet water temperature difference (about 0.2 °C) is not significant as well as heat extract capacity. However, the BHE system COP could reach the peak value (15.9) when the outer diameter of inner pipe is 0.11 m. That is because the flow resistance under this condition is the lowest as shown in Fig. 13(b). In the meantime, the pressure difference between inlet and outlet is the lowest (1.47 Mpa) which means the circulating pump power is also the lowest (17.3 kW) as well as the corresponding water head (147.5 m). Fig. 13 reveals that the inner pipe diameter would not influence the heat extract capacity of BHE significantly, but there is an optimal inner pipe diameter (outer diameter: 0.11 m) to minimize flow resistance and pump power.

Fig. 13. (a) Influence of inner pipe diameter on the temperature difference between outlet and inlet, heat extract capacity, and COP_{BHE} . **(b)** Influence of inner pipe diameter on corresponding water head, water pressure difference between inlet and outlet, and circulating pump power.

The outer surface of the outer pipe is the main heat extract surface to absorb heat from the rock-soil. Thus, the outer pipe diameter would not only influence the flow resistance but also the thermal performance of BHE. Thus, the influence of outer pipe diameter has been further studied under these working conditions: the inner pipe diameter is 0.11 m, circulating water mass flow rate is 12 kg/s, inlet water temperature to BHE is 20 °C and depth of BHE is 2500 m. As shown in Fig. 14(a), the temperature difference between outlet and inlet and the heat extract capacity both increase gradually with the increase of outer pipe diameter while the BHE system COP increases rapidly at first and then increase smoothly. The outlet water temperature could reach 28.3 °C when the outer pipe diameter is 0.378 m. Fig. 14(b) shows that a larger outer pipe diameter would reduce the flow resistance, thus, the circulating pump power, as well as corresponding water head, are lower under a larger outer pipe diameter. For instance, the pressure difference between inlet and outlet is the lowest (0.78 Mpa) while the pump power is 9.2 kW. Therefore, a larger outer pipe diameter has a larger heat transfer surface area which is better for the circulating water to extract heat from the rock-soil. Moreover, a larger outer pipe diameter could also reduce the flow resistance and circulating pump power.

(a)

(b)

Fig. 14. (a) Influence of outer pipe diameter on the temperature difference between outlet and inlet, heat extract capacity, and COP_{BHE} . **(b)** Influence of outer pipe diameter on corresponding

water head, water pressure difference between inlet and outlet, and circulating pump power.

5.4 Thermal effect radius

Thermal effect radius is an important parameter to determine the arrangement of several borehole heat exchangers. The heat extract capacity would be degraded and the recovery of ground temperature would be affected if the BHEs are placed too closely. Fig. 15 reveals the variation trends of the thermal effect radius of BHE at different depths. The simulation results show that the thermal effect radius would decrease at first when the depth is less than 750 m and then increase when the depth is bigger than 750 m. That is because when circulating water flow through the outer pipe, it will be heated by the rock-soil and the temperature difference between inlet and outlet water would decrease when the depth is less than 750 m. The circulating water will extract less heat from the rock-soil and cause a smaller thermal effect radius. The biggest thermal effect radius is less than 8 m which means if the distance of two BHEs is larger than 16 m, the effect between the two BHEs could be neglected.

Fig. 15. Thermal effect radius of BHE at different depths.

5.5 Solar radiation intensity

Fig. 16 shows the influence of solar radiation intensity varying from 200 W/m² to 1000 W/m² on circulating water temperature, heating area, and solar fraction. The working conditions are: area of PV/T module is 1000 m²; depth of BHE is 2500 m; mass flow rate of circulating water is 12 kg/s and ambient temperature is 10 °C. The inlet water temperature is 30 °C while the temperature difference between inlet and outlet circulating water is 3.5 °C, thus, the outlet water temperature is 33.5 °C. The temperature range of circulating water for heating applications is from 35 °C to 45 °C while 33.5 °C is not high enough for residential heating. The solar assisted PV/T heat pump system is adopted to further heat the circulating water. The temperature increments by the PV/T heat pump as well as the heating COP increase with the increase of solar radiation intensity. Solar fraction is an important parameter to evaluate the contribution of solar energy. The solar assisted PV/T heat pump system could increase 3.2 °C of the outlet water temperature from BHE when solar radiation intensity is 200 W/m² and the circulating water could be heated up to 36.7 °C while the solar fraction

is 47.5%. The temperature increment by the PV/T heat pump could reach 7.3 °C and the outlet water to users could be heated up to 40.8 °C if the solar radiation intensity is 600 W/m². In this case, the solar fraction is 67.5% while the heating COP of this hybrid system is 7.4. The borehole heat exchanger coupled with a solar assisted PV/T heat pump heating system is thus a promising technology for residential heating due to high efficiency, low energy consumption, and environmental-friendly.

Fig. 16. Influence of solar radiation intensity on circulating water temperature, heating COP of this hybrid system, and solar fraction.

One merit of the PV/T module is that it could produce electricity and heat simultaneously, thus, the electricity generated by PV panels could be used for system consumption including compressor and pump. The pump power using in this hybrid system is 17.3 kW when the mass flow rate is 12 kg/s while the compressor power is simulated through the mathematical model. The influence of solar radiation intensity on output power to grid, heating power produced by BHE, heating power produced by heat pump, and overall heating power has shown in Fig. 17. The output power to grid, heating power produced by solar assisted PV/T heat pump, and overall heating power increase linearly with the increase of solar radiation intensity. The electricity generated by PV panels could meet the energy consumption demand of this hybrid system when solar radiation intensity exceeds 600 W/m².

Fig. 17. Influence of solar radiation intensity on output power to grid, heating power produced by BHE, heating power produced by heat pump, and overall heating power.

5.6 Area of PV/T module

Fig. 18 presents the influence of the area of PV/T module varying from 200 m² to 2000 m² on circulating water temperature, heating area, and solar fraction. The working conditions are given: solar radiation intensity is 600 W/m²; the depth of BHE is 2500 m; the mass flow rate of circulating water is 12 kg/s and the ambient temperature is 10 °C. The temperature increment by PV/T heat pump increases linearly with the increase of the area of PV/T module due to a larger solar absorption surface. The heating COP of this hybrid system decreases and solar fraction increases with the increase of PV/T area. The outlet water temperature from this hybrid system is 35 °C which is in the temperature range for residential heating when the area of PV/T module is 200 m². The solar fraction could reach 80.6% when the area of PV/T module is 2000 m². In the meantime, the outlet water temperature could reach 48 °C. The heating COP of this hybrid system decreases from 8.7 to 7.0 when PV/T area varies from 200 m² to 2000 m².

Fig. 18. Influence of area of PV/T module on circulating water temperature, heating COP of this hybrid system, and solar fraction.

The influence of the area of PV/T module on output power to grid, heating power produced by BHE, heating power produced by heat pump, and overall heating power has shown in Fig. 19 and the solar radiation intensity is 600 W/m². The variation curves show the same linearly increasing trend as in Fig. 18. The maximum overall heating power is 908 kW while 80.6% of it produced by the heat pump when the area of PV/T module is 2000 m². The output power to grid exceeds zero when PV/T module's area over 650 m² which means the electricity produced by PV panels could meet system demand. Moreover, the surplus power could be sold to the electrical grid to create economic benefits for users.

Fig. 19. Influence of area of PV/T module on output power to grid, heating power produced by BHE, heating power produced by heat pump, and overall heating power.

5.7 Feasibility analysis

A comparison between a single BHE heating system and a BHE coupled with solar PV/T heat pump heating system should be conducted to show the feasibility and merits of this hybrid system. Thus, the performance comparison in detail has been listed in Table. 8 under typical working conditions which have shown in Table. 7.

Table. 7. Typical working conditions.

Parameters	Nomenclature	Value	Unit
Depth of BHE	H	2500	m
Mass flow rate of circulating water	m	12	kg/s
Inlet water temperature to BHE	T_i	30	°C
Area of PV/T module	$A_{PV/T}$	1000	m²
Solar radiation intensity	I	600	W/m²
Ambient temperature	T_a	10	°C
Ground surface temperature	T_{up}	10	°C
Wind velocity	v_w	1.5	m/s

Table. 8 presents the comparison results between a single BHE heating system and a BHE coupled with solar PV/T heat pump heating system. The heating power of this hybrid system is 542 kW which is about 3 times of a single BHE system. The outlet water temperature from BHE could increase 7.3 °C after heating by solar assisted PV/T heat pump. This hybrid system would consume 56.4 kW electricity to drive the compressor, however, the PV/T module could produce 83.1 kW electricity through PV panels which could meet the energy demand of the compressor and pump. Thus, this hybrid system could realize self-operation under this condition.

Table. 8. Performance comparison between single BHE heating system and BHE coupled with PV/T heat pump heating system.

Parameters	Single BHE heating system	BHE coupled with PV/T heat pump heating system
Heating power (kW)	176.4	542.3
Outlet water temperature (°C)	33.5	40.8
Circulating pump power (kW)	17.3	17.3
Compressor power (kW)	0	56.4
Total energy consumption power (kW)	17.3	73.7
Electricity generation power (kW)	0	83.1
Heating COP (-)	10.2	7.4

Fig. 20 shows the contribution ratio of BHE, solar energy, and heat pump in the residential heating power of this hybrid system. The total heating power produced by this hybrid system is 542 kW, the heating power produced by solar energy accounts for 57% of it due to the absorption heat from PV/T module. The heating power produced by BHE and the heating power produced by the heat pump are 33% and 10% of total heating power, respectively. Hence, this residential heating system using BHE coupled with a solar assisted PV/T heat pump has a significant improvement in thermal performance compared with a single BHE heating system. Therefore, the combination of a borehole heat exchanger and the solar assisted PV/T heat pump has broad application prospect and potential usage in stable, comfortable, low-energy consumption, and environmental-friendly residential heating.

Fig. 20. Contribution ratio of BHE, solar energy, and heat pump in residential heating power.

6 Conclusion

The performance analysis of a residential heating system using a borehole heat exchanger coupled with a solar assisted PV/T heat pump has been conducted. It is aiming to optimize the performance and demonstrates the merits of this hybrid system. The effects of the system's physical structure parameters and operating conditions have been also numerically investigated. The main conclusions can be drawn as follows:

(1) The outlet water temperature as well as the BHE system COP decrease and the heat extract capacity as well as flow resistance increase with the increase of mass flow rate. The maximum heat extract capacity is 282.5 kW while the BHE system COP is 7.3 when the mass flow rate is 16 kg/s. In addition, the circulating water could not extract heat from BHE if the inlet water temperature

exceeds 48.5°C when the mass flow rate is 12 kg/s.

(2) The inner pipe diameter would not influence the heat extract capacity of BHE significantly, but there is an optimal inner pipe diameter (outer diameter: 0.11 m) to minimize the flow resistance (1.47 Mpa) and the pump power (17.3 kW) when the outer pipe diameter is 0.178 m. Larger outer pipe diameter is better for the circulating water to extract heat from the rock-soil and it could also reduce the flow resistance and the circulating pump power.

(3) The maximum outlet temperature could reach 40.8 °C while the solar fraction is 67.5% when the area of PV/T module is 1000 m² and solar irradiation is 600 W/m². In addition, the electricity generated by the PV panels could meet the system's energy consumption demand when solar irradiation exceeds 600 W/m² or PV/T module's area is larger than 650 m². Moreover, the heating COP of this hybrid system could reach 7.4 which is higher than that of a conventional heating system.

Therefore, the analysis of the above-mentioned parameters could be used to design and optimize the residential heating system using borehole heat exchanger coupled with a solar assisted PV/T heat pump.

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Nomenclature:

Symbols

A	area (m ²)
F'	unmodified efficiency factor (-)
H	depth of borehole heat exchanger (m)
h	heat transfer coefficient (W/m ² ·°C)
U	heat loss coefficient (W/m ² ·°C)
V	volume flow rate (m ³ /h)
r	radius (m)
d	diameter (m)
T	temperature (K)
I	solar radiation intensity (W/m ²)
Q	heat transfer rate (W)
W	power (W)
v	velocity (m/s)
k	thermal conductivity (W/m·°C)
m	mass flow rate (kg/s)
n	numbers (-)
C_p	specific heat at constant pressure (kJ/kg·°C)
R	thermal resistance (m·°C/W)

Greek symbols

δ	thickness (m)
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τ	transmittance (-)
a	absorption ratios (-)
β	packing factor (-)
ε	emissivity (-)
η	efficiency (-)
ρ	density (kg/m ³)

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647 Subscripts

p	PV panels
$pump$	pump
$heating$	residential heating
e	electrical
c	PV-glazing cover
ref	refrigerant
res	flow resistance
cv	convection
cd	conduction
rd	radiation
a	ambient
L	lost
u	useful
f	fluid
Tot	total

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